# CFD SIMULATION OF HEAT TRANSFER IN VERTICAL RIBBED TUBE 

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#### Abstract

Computational Fluid Dynamics (CFD) simulation of heat transfer and fluid flow analysis in the turbulent flow regime in a spirally ribbed tube and a smooth tube in vertical orientation are simulated in this project using ANSYS Fluent. The ribbed tube has outside diameter of 25 mm , maximum inner diameter of 18.80 mm , minimum inner diameter of 17.50 mm and pitch varied from 2 m to 0.25 m . The smooth tube has outside diameter of 26.7 mm and inner diameter of 18.88 mm . Both tubes were uniformly heated by passing an electrical current along the tube with a heated length of 1m. The CFD simulation is performed on a vertical orientation of the steel tubes (rifled and smooth) under six different inlet velocities of $0.893 \mathrm{~m} / \mathrm{s}, 1.786 \mathrm{~m} / \mathrm{s}, 2.38 \mathrm{~m} / \mathrm{s}, 2.976 \mathrm{~m} / \mathrm{s}, 3.57 \mathrm{~m} / \mathrm{s}$ and $4.166 \mathrm{~m} / \mathrm{s}$. The main objective of this thesis is to determine the heat transfer and pressure drop in both vertical smooth and ribbed tubes. The fluid used is water and the initial temperature is $25^{\circ} \mathrm{C}$. The heat flux that for heating the tube is equal to $150 \mathrm{KW} / \mathrm{m}^{2}$. During the CFD simulation analysis it was found that for smooth tube at lower inlet velocity, the temperature increases from 298 K to 310.4 K while the pressure drop between inlet and outlet is equal to 598 Pa . At higher inlet velocity, the temperature for smooth tube is found increasing from 298 K to 301.53 K , with the pressure drop is equal to 7368.1 Pa . Smooth tubes results are validated again analytical calculation, it is agreed well with analytical results. For the ribbed tube at lower inlet velocity the temperature is increasing from 298 K to 313.5 K , with the pressure drop is found to be $\mathbf{6 2 2 . 1} \mathrm{Pa}$ for 0.25 m pitch. In the case of a higher inlet velocity, the temperature increase in ribbed tube is increasing from 298 K to 304.5 K , while the pressure drop is equal to 8087.1 Pa . It is clear that the temperature difference between ribbed and smooth tube at lower inlet velocity are equal to 15.5 K and 12.4 K , respectively. While at higher inlet velocity there, temperature difference becomes 6.5 K , and 3.5 K respectively. This result indicates that the ribbed tube has higher heat transfer efficiency than the smooth tube. The pressure drop in the ribbed tube is found to be higher than that of the smooth tube. This clearly shows that the characteristic of ribbed tube is much better than smooth tube.


Keyword: Computational Fluid Dynamics, Computation Heat Flux Helix, angle Specific heat, Pressure.

## 1. INTRODUCTION

The problem of heat and mass transfer enhancement plays a dominant role in designing and manufacturing new energy systems, power plant devices, air conditioning equipment and heat exchangers. Among lots of augmentation techniques, flow swirling is the most simple, reliable and frequently used method of heat transfer enhancement in circular tubes. It is widely used in ducts of nuclear power stations, heat exchangers, refrigerators, radiators, airplane and space devices the proper designs of the tube inner wall will increase the heat transfer to the flowing water; hence it is one of the main factors for its successful usage in boiler. In order to increase the heat transfer and prevent damage to the inner wall of tube, ribbed tubes are applied instead of the smooth walled tubes. The heat transfer coefficient is one of the most important factors for the successful design and operation of inner tube wall to heat transfer on the flowing water. Analysis and modeling of the inner tube wall for boiler is very important, in order to keep the boiler operation below the critical stages.

In recent years, the high cost of energy and material has results an increased effort for producing more efficient heat exchange equipment. The design procedure of heat exchangers is quite complicated, as it needs exact analysis of heat transfer rate and pressure drop.

## 2. OBJECTIVE AND SCOPE OF WORK

### 2.1 Objectives of Study

1. To determine the fluid flow characteristics in a vertical positioned tube (smooth and ribbed) by means of CFD.
2. To determine the heat transfer in a vertical tube (smooth and ribbed) by means of Computational Fluid Dynamics
(CFD).
3. To determine the pressure drop in a Vertical tube (smooth and ribbed) by means of Computational Fluid Dynamics (CFD).

### 2.2 Scope of Study

Computational Fluid Dynamics (CFD) will be used to determine the characteristics of fluid flow in the ribbed and smooth tube.

1. Water will be used as the fluid domain in Computational Fluid Dynamics (CFD).
2. Steel tube, (smooth and ribbed) will be analyzed by using Computational Fluid Dynamics (CFD).
3. The analysis by using Computational Fluid Dynamics (CFD) will be conducted with tubes placed vertical.
4. The fluid flow in this analyzed will be single phased.

## 3. Geometry of smooth tube and ribbed tube

The commercial CFD code FLUENT 13.0 is used to analyze the model flow characteristics of smooth and ribbed tube. Modeling and mesh generation are however performed in ANSYS Design Modeler and ANSYS Meshing environment. Water is taken as the fluid medium. The schematic diagram of the smooth tube model show in figure 4.1, that comprise an outer diameter is 26.7 mm , Inner diameter is 18.88 mm , the wall thickness is 3.91 mm , and the length of smooth tube is 1 m .

Figure 4.1 shows the schematic diagram of the ribbed tube model that comprises a 25 mm outer diameter, 18.8 mm maximum inlet diameter and 17.5 mm minimum inlet diameter. The length of the tube 1 m , the rib height is 0.6835 mm and the width is 9.25 mm . The helix angle is 60 o , and the number of starts is 4 . The ribbed tube parameter used in this analysis is show in table 4.1. In this study the effect of helix pitch from 2 m to 0.25 m is studied. Fig. 4.3 to 4.8 shows the Geometric model of ribbed tube Helix pitch 2 m to 0.25 m .


Fig 3. 3 Geometric model of ribbed tube Helix pitch 1 m and .25 m

## 4 Boundary conditions

The present work set both the tubes is sited vertically and the flow inside the tube is assumed as fully turbulent flow. The water temperature is set at $25^{\circ} \mathrm{C}\left(298^{\circ} \mathrm{K}\right)$, with water properties at that temperature as shown in the table 3.3 . Figure 3.5 shows the prescribed boundary condition for solving this flow problem numerically by using Fluent software. In that figure, q is representing the heat flux at constant rate which created by passing an electrical current ( $150 \mathrm{KW} / \mathrm{m} 2$ ) along 1 meter tube length. At the inlet station, the water velocity can be set for different value. The present study carries out six different inlet velocities at constant inlet temperature 25 oC . Those six inlet velocities are: $0.893,1.786,2.38,2.976,3.57$ and $4.166 \mathrm{~m} / \mathrm{s}$.

Table 4.1 the properties of water at temperature at $\left(298{ }^{\circ} \mathrm{K}\right)$.

| Tempature <br> (I) | $\begin{aligned} & \text { Dexity } \\ & \text { p(kint } \end{aligned}$ | Spaiflcuat (pilgrif | Themal mandurity bivink | Dymic Thasity Hfonges |
| :---: | :---: | :---: | :---: | :---: |
| 28 | 99.1 | 4180 | 0.6035 | 0.0069 |



Fig 4.5 Boundary conditions, (a) ribbed tube, (b) smooth tube.
The tube uses a steel material and it had been found the material properties are a constant if the steel operated below $300{ }^{\circ} \mathrm{K}$ and they will vary if the temperature above of it. The steel properties in term of density, the specific heat coefficient at constant pressure $C p$ and thermal conductivity $k$ below $300{ }^{\circ} \mathrm{K}$ are shown in the Table. 4.3

## 6. Results Smooth tube- Velocity $0.83 \mathrm{~m} / \mathrm{s}$

The CFD analysis studies by use of fluent software for the flow along the tube with heat transfer effects are presented. The CFD analysis applied for the case of internal flow problems through a vertically positioned smooth and ribbed tube in order to determine the heat transfer and pressure drop along the tube. Comparison result among of them will be carried out to determine the most suitable tube model in handling the heat transfer problem.

CFD simulation study was carried out using the smooth tube with six different inlet velocities at constant temperature $\left(25^{\circ} \mathrm{C}\right)$ and heat flux ( $150 \mathrm{KW} / \mathrm{m}^{2}$ ). The result of Pressure shows 4.12 the linear variation in pressure drops from inlet to outlet.


Fig.4. 3 Pressure contours of smooth tube- Velocity $0.83 \mathrm{~m} / \mathrm{s}$


Fig.4. 4 Total Pressure contours of smooth tube- Velocity $0.83 \mathrm{~m} / \mathrm{s}$
It is clear from figure 4.14 that the temperatures along the tube increased for all cases, but the highest temperature increment occurs at the small inlet velocity. At the inlet velocity equals to $0.893 \mathrm{~m} / \mathrm{s}$, the temperature rises from 298 K to 310 K , while at a higher inlet velocity, namely at velocity $4.166 \mathrm{~m} / \mathrm{s}$, the temperature increment is only 1 degree is from, 298 K , to 301.53 K . This result indicates that a lower inlet velocity is better than a higher inlet velocity.
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Fig.4. 5 Velocity contours of smooth tube- Velocity $0.83 \mathrm{~m} / \mathrm{s}$

### 4.8 Results Inlet Velocity $\mathbf{2 . 3 8} \mathbf{~ m} / \mathrm{s}$

The result of Pressure shows 4.16 the linear variation in pressure drops from inlet to outlet for Velocity $2.38 \mathrm{~m} / \mathrm{s}$. The Pressure drop approximately 3532 Pa


Fig.4. 6 Pressure contours of smooth tube- Velocity 2.38 m/s.


Fig.4. 7 Total Pressure contours of smooth tube- Velocity $2.38 \mathrm{~m} / \mathrm{s}$
It is clear from figure 4.18 that the temperatures along the tube increased for all cases, but the highest temperature increment occurs at the small inlet velocity. At the inlet velocity equals to $0.2 .38 \mathrm{~m} / \mathrm{s}$, the temperature rises from 298 K to 303.23 K , while
at a higher inlet velocity, namely at velocity $4.166 \mathrm{~m} / \mathrm{s}$, the temperature increment is only 3.5 degree is from, 298 K , to 301.53 K . This result indicates that a lower inlet velocity is better than a higher inlet velocity.


Fig.4. 8 Velocity contours of smooth tube- Velocity 2.38 m/s


Fig.4. 9 Smooth Tube CFD and analytical Comparison of Pressure drop Vs velocity

## Results Ribbed Tube

Table.5.1 Comparison of Pressure drop and Temperature Outlet

| S.No | Velocity <br> $\mathrm{m} / \mathrm{s}$ | Helix Pitch <br> mm | Pressure <br> drop Pa | Temperature <br> Outlet K |
| ---: | ---: | ---: | ---: | ---: |
| 0 | 0.893 | 2000 | 622.1769 | 313.5464 |
| 1 | 1.786 | 2000 | 2182.804 | 308.0692 |
| 2 | 2.38 | 2000 | 3674.174 | 306.2633 |
| 3 | 2.976 | 2000 | 5509.847 | 305.225 |
| 4 | 3.57 | 2000 | 7662.782 | 304.5443 |
| 5 | 0.893 | 1500 | 635.5347 | 314.7031 |
| 6 | 1.786 | 1500 | 2219.131 | 308.4056 |
| 7 | 2.38 | 1500 | 3732.504 | 306.605 |
| 8 | 2.976 | 1500 | 5595.369 | 305.5384 |
| 9 | 3.57 | 1500 | 7773.213 | 304.8327 |
| 10 | 0.893 | 1000 | 649.2463 | 315.0022 |
| 11 | 1.786 | 1000 | 2246.4 | 308.6995 |
| 12 | 2.38 | 1000 | 3806.698 | 306.889 |
| 13 | 2.976 | 1000 | 5702.821 | 305.8224 |
| 14 | 3.57 | 1000 | 7933.464 | 305.1241 |
| 15 | 0.893 | 750 | 663.9655 | 315.6399 |
| 16 | 1.786 | 750 | 2313.487 | 309.3095 |


| 17 | 2.38 | 750 | 3887.84 | 307.5036 |
| ---: | ---: | ---: | ---: | ---: |
| 18 | 2.976 | 750 | 5824.368 | 306.4389 |
| 19 | 3.57 | 750 | 8093.217 | 305.7453 |
| 20 | 0.893 | 500 | 738.7884 | 316.2625 |
| 21 | 1.786 | 500 | 2575.044 | 309.8678 |
| 22 | 2.38 | 500 | 4331.424 | 308.0796 |
| 23 | 2.976 | 500 | 6492.072 | 307.0261 |
| 24 | 3.57 | 500 | 9024.9 | 306.3372 |
| 25 | 0.893 | 250 | 863.6719 | 316.5687 |
| 26 | 1.786 | 250 | 2998.398 | 310.2409 |
| 27 | 2.38 | 250 | 5040.178 | 308.4297 |
| 28 | 2.976 | 250 | 7555.756 | 307.3527 |
| 29 | 3.57 | 250 | 10513.19 | 306.6499 |

## 7. Ribbed Tube-Helix Pitch 2 m -Velocity $0.83 \mathrm{~m} / \mathrm{s}$



Fig.5. 1 Pressure contours of ribbed tube-Helix Pitch 2 m - Velocity $\mathbf{0 . 8 3} \mathbf{~ m} / \mathrm{s}$


Fig.5. 2 Total Pressure contours of ribbed tube-Helix Pitch 2m-Velocity $\mathbf{0 . 8 3} \mathbf{~ m} / \mathrm{s}$


Fig.5. 3 Velocity contours of ribbed tube-Helix Pitch 2 m -Velocity $\mathbf{0 . 8 3} \mathbf{~ m} / \mathrm{s}$.
5.2 Ribbed Tube-Helix Pitch $\mathbf{2 m}$-Velocity $2.38 \mathrm{~m} / \mathrm{s}$


Fig.5. 4 Pressure contours of ribbed tube-Helix Pitch 2 m - Velocity $2.38 \mathrm{~m} / \mathrm{s}$


Fig.5. 5 Total Pressure contours of ribbed tube-Helix Pitch 2m-Velocity 2.38 m/s


Fig.5. 6 Velocity contours of ribbed tube-Helix Pitch 2 m -Velocity $2.38 \mathrm{~m} / \mathrm{s}$

Ribbed Tube-Helix Pitch 1m -Velocity $0.83 \mathrm{~m} / \mathrm{s}$


Fig.5. 7 Pressure contours of ribbed tube-Helix Pitch 1 m - Velocity $0.83 \mathrm{~m} / \mathrm{s}$.


Fig.5. 8 Total Pressure contours of ribbed tube-Helix Pitch 1 m-Velocity $0.83 \mathrm{~m} / \mathrm{s}$.


Fig.5. 9 Velocity contours of ribbed tube-Helix Pitch $1 \mathbf{m}$-Velocity $0.83 \mathrm{~m} / \mathrm{s}$
5.6 Ribbed Tube-Helix Pitch 1m -Velocity $2.38 \mathrm{~m} / \mathrm{s}$


Fig.5. 10 Pressure contours of ribbed tube-Helix Pitch 1 m-Velocity 2.38 m/s.


Fig.5. 11 Total Pressure contours of ribbed tube-Helix Pitch 1m-Velocity 2.38 m/s


Fig.5. 12 Velocity contours of ribbed tube-Helix Pitch 1 m -Velocity $2.38 \mathrm{~m} / \mathrm{s}$

Ribbed Tube-Helix Pitch 0.25 m -Velocity $0.83 \mathrm{~m} / \mathrm{s}$


Fig.5. 13 Pressure contours of ribbed tube-Helix Pitch 0.25 m - Velocity $0.83 \mathrm{~m} / \mathrm{s}$
5.12 Ribbed Tube-Helix Pitch 0.25 m -Velocity $2.38 \mathrm{~m} / \mathrm{s}$


Fig.5. 14 Pressure contours of ribbed tube-Helix Pitch 0.25 m - Velocity 2.38 m/s


Fig.5. 15 Total Pressure contours of ribbed tube-Helix Pitch 0.25 m-Velocity 2.38 m/s


Fig.5. 16 Velocity contours of ribbed tube-Helix Pitch 0.25 m -Velocity $2.38 \mathrm{~m} / \mathrm{s}$

## Graphs and Comparison



Fig.5. 17 Comparison Pressure Drop Vs Velocity
Fig.5.49 demonstrates the numerical and analytical results for the pressure drop vs. velocity number for different types of helix pitch from 2 m to 0.25 m . The ribbed tube results are represented using solid lines, while the corresponding analytical results are denoted by circular " + " symbols. It was found that the pressure drop for ribbed was $10-60 \%$ higher than that of plain tubes and that of 0.25 m helix pitch shows $25-60 \%$ higher.


Fig.5. 18 Comparison Outlet temperature Vs Velocity
Fig.5.49 demonstrates the numerical and analytical results for the Outlet temperature vs. velocity number for different types of helix pitch from 2 m to 0.25 m . The ribbed tube results are represented using solid lines, while the corresponding analytical results are denoted by circular " + " symbols. It was found that the temperature rise for ribbed was $10-40 \%$ higher than that of plain tubes and that of 0.25 m helix pitch shows $25-40 \%$ higher.

## CONCLUSIONS

Computational Fluid Dynamics (CFD) analysis of heat transfer and fluid flow analysis in the turbulent flow regime in a spirally ribbed tube and a smooth tube in vertical orientation are investigated using ANSYS Fluent. The Geometric model of the ribbed and smooth tube is created using ANSYS Design Modeler. CFD meshing is carried out using ANSYS Meshing Platform. The CFD simulation is performed on a vertical orientation of the steel tubes (rifled and smooth) under six different inlet velocities of $0.893 \mathrm{~m} / \mathrm{s}, 1.786 \mathrm{~m} / \mathrm{s}, 2.38 \mathrm{~m} / \mathrm{s}, 2.976 \mathrm{~m} / \mathrm{s}, 3.57 \mathrm{~m} / \mathrm{s}$ and $4.166 \mathrm{~m} / \mathrm{s}$. The main objective of this thesis is to determine the heat transfer and pressure drop in both vertical smooth and ribbed tubes. The fluid used is water and the initial temperature is $25^{\circ} \mathrm{C}$. The heat flux that for heating the tube is equal to $150 \mathrm{KW} / \mathrm{m}^{2}$.

## REFERENCES

[1] Lixin Cheng and Tingkuan Chen, Flow boiling heat transfer in a vertical spirally internally ribbed tube, HEAT AND MASS TRANSFER Volume 37, Numbers 2-3 (2001), 229-236, DOI: 10.1007/PL00013294
[2] Wang, Weishu; Bi, Qincheng; Gu, Hongfang; Chen, Tingkuan; Luo, Yushan, An Investigation on Heat Transfer to Water Flowing in Vertical Upward Internally Ribbed Enhancement Tube at Supercritical Pressure, Advanced Science Letters, Volume 4, Numbers 6-7, June/July 2011, pp. 2281-2288(8)
[3] Ooi, G. Iaccarino, P.A. Durbin, M. Behnia Reynolds averaged simulation of flow and heat transfer in ribbed ducts, International Journal of Heat and Fluid Flow 23 (2002) 750-757.
[4] Abdulati Muftah Mohamed Ibrahim, Bashir Rahuma Elhub, H. Abas A. Wahab, Experimental Study on Heat Transfer and Fluid Flow in Vertical Rifled, Advanced Materials Research (Volume 505), April, 2012.
[5] L. Cheng ${ }^{1}$, T. Chen, Enhanced Heat Transfer Characteristics of Upward Flow Boiling of Kerosene in a Vertical Spirally Internally Ribbed Tube, Chemical Engineering \& Technology Volume 29, Issue 10, pages 1233-1241, October, 2006.

